

Engineering the Interface and Interaction Structure on Highly Coke-Resistant Ni/CeO₂-Al₂O₃ Catalyst for Dry Reforming of Methane

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Table S1. Textural Properties of NiO/Al₂O₃ and NiO/CeO₂-Al₂O₃

Catalyst	S_{BET} (m ² ·g ⁻¹)	V_p (cm ³ ·g ⁻¹)	D_p (nm)
NiO/Al ₂ O ₃	171	0.7	16.3
NiO/CeO ₂ -Al ₂ O ₃	197	0.8	16.1

Table S2. Results of H₂ Chemisorption for Ni/Al₂O₃ and Ni/CeO₂-Al₂O₃

Catalyst	H ₂ uptake (m ³ /g)	Dispersion (%)	S _{Ni} (m ² /g)	d _{Ni} (nm)
Ni/Al ₂ O ₃	1.10	6.5	54.8	7.7
Ni/CeO ₂ -Al ₂ O ₃	1.13	6.5	55.0	6.5

Table S3. Comparison of CH₄ and CO₂ Conversions as Well as Coke Deposition Rate with Other Catalysts in DRM

Catalysts	Temperature (°C)	GHSV (mL g _{cat} ⁻¹ h ⁻¹)	Ratio of feed gases	CH ₄ conversion (%)	CO ₂ conversion (%)	Stability (h)	Coke deposition rate (mg _c g _{cat} ⁻¹ h ⁻¹) ^a	Ref.
Ni/CeO ₂ -Al ₂ O ₃	500	24,000	CH ₄ /CO ₂ = 1/1	12	16	50	0.42	This work
NiFe/Al ₂ O ₃	450	12,000	CH ₄ /CO ₂ = 1/1	9.6	14	20	1.18	1
Pt ^{0.25} -NiCe@SiO ₂	500	60,000	CH ₄ /CO ₂ /N ₂ = 1/1/1	~6.5	~11.5	20	1.81	2
Ni-Co/La ₂ O ₃	650	119,000	CH ₄ /CO ₂ /N ₂ = 45/45/10	30	40	10	100	3
0.3PdNi/MCM-41	550	120,000	CH ₄ /CO ₂ /N ₂ = 1/1/3	38	52	12	156.8	4
NMG-600	600	54,000	CH ₄ /CO ₂ /N ₂ = 1/1/1	48	52	12	1.44	5
1Ni2Co/ZSM5	700	60,000	CH ₄ /CO ₂ /Ar = 1/1/3	69	60	12	28.69	6
0.5Ru@Ni-MCM-41	600	36,000	CH ₄ /CO ₂ /Ar = 1/1/1	35	38	4	485.29	7
Ni-Ce _{1-x} Zr _x O ₂ _cp	600	60,000	CH ₄ /CO ₂ /Ar = 1/1/8	55	70	24	684	8
75Ni25Co-Al-5Ca	600	7,000	CH ₄ /CO ₂ /N ₂ = 1/1/3	19	57	3.5	37.7	9
Ni@SBA-15-EG	750	7,500	CH ₄ /CO ₂ = 1/1	45	35	20	1.975	10

a carbon deposition rate: $R_c = \frac{m_c}{m_{cat} \cdot \text{time (h)}}$, where m_c and m_{cat} represent the amounts of carbon on the spent catalyst and the mass of catalyst, respectively.

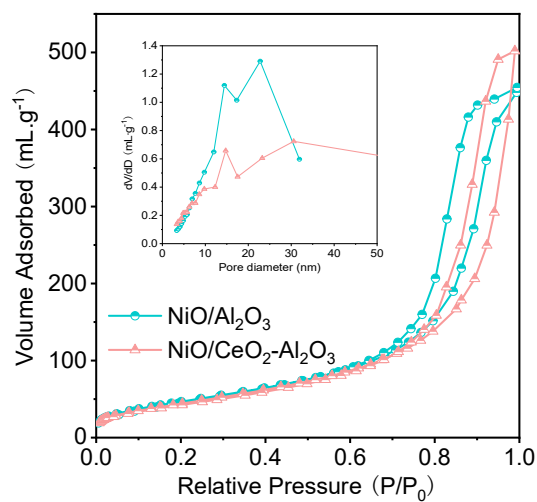


Figure S1. N₂ isotherms of fresh NiO/Al₂O₃ and NiO/CeO₂-Al₂O₃.

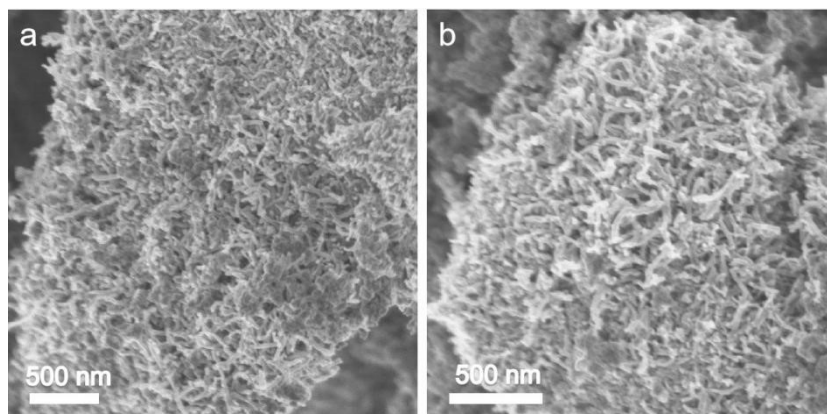


Figure S2. SEM images of the control NiO/CeO₂-Al₂O₃ catalyst after stability test.

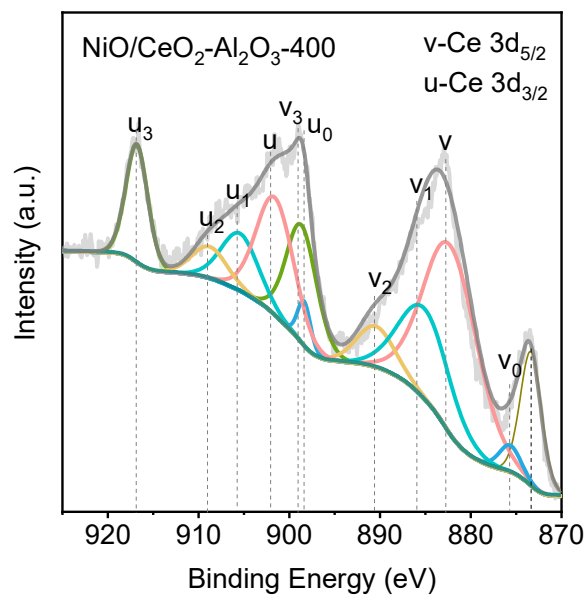


Figure S3. Ce 3d XPS spectra of the control NiO/CeO₂-Al₂O₃ catalyst.

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